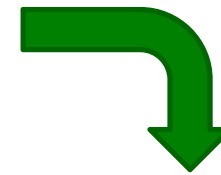
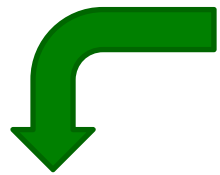
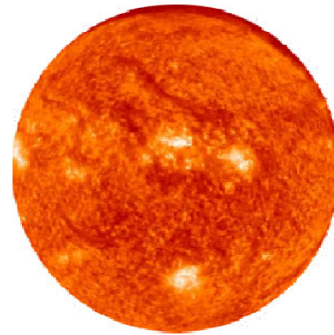


# ARPA-E Electrofuels Program Meeting & Workshop

Ramon Gonzalez  
Program Director  
ARPA-E

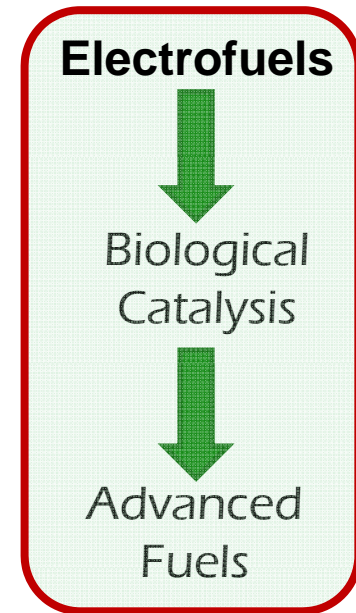
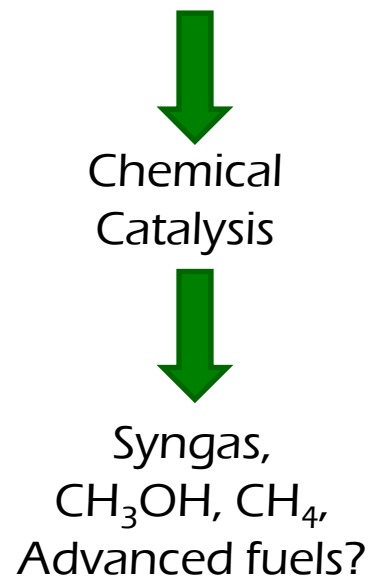
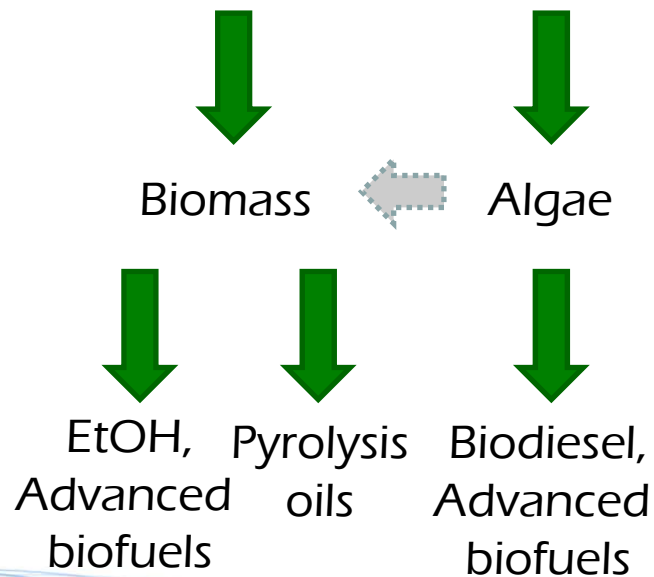
December 10, 2012  
Houston, Texas

# Original vision of the program focused on the opportunity to utilize renewable electrons to power Electrofuels production...

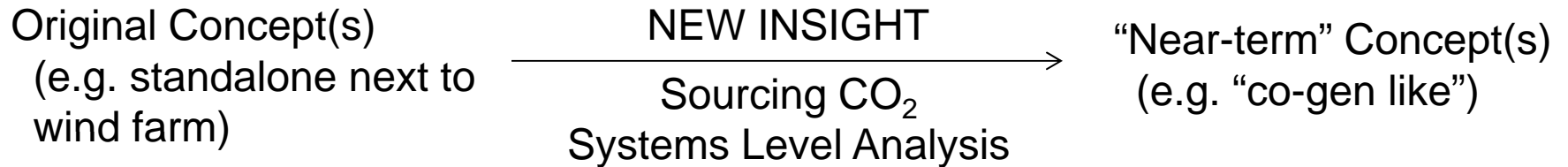


Photosynthesis

Electrons/  
Reducing equivalents



## Strategic vision has evolved as the program has matured and new insights have come to light



Originally vision of CO<sub>2</sub> sourced from coal/NG electricity production

- Systems level analysis suggests this is an inefficient way to GTL/CTL
- Also not likely to qualify as a biofuel

### Electricity & CO<sub>2</sub>

1. Biofuels production releases up to 1/3 of total carbon feedstock as CO<sub>2</sub>
  - e.g. Sugar-to-fuel fermentation releases 2/6 carbon from every sugar molecule
  - Extremely pure and concentrated CO<sub>2</sub> stream
2. CO<sub>2</sub> from geothermal could enable Iceland/Japan to become “oil” producers

### H<sub>2</sub> & CO<sub>2</sub>

1. GTL/XTL using Electrofuels to convert CO<sub>2</sub>/H<sub>2</sub> into fuel
2. Opportunity to couple fuel and ammonia production in same reactor

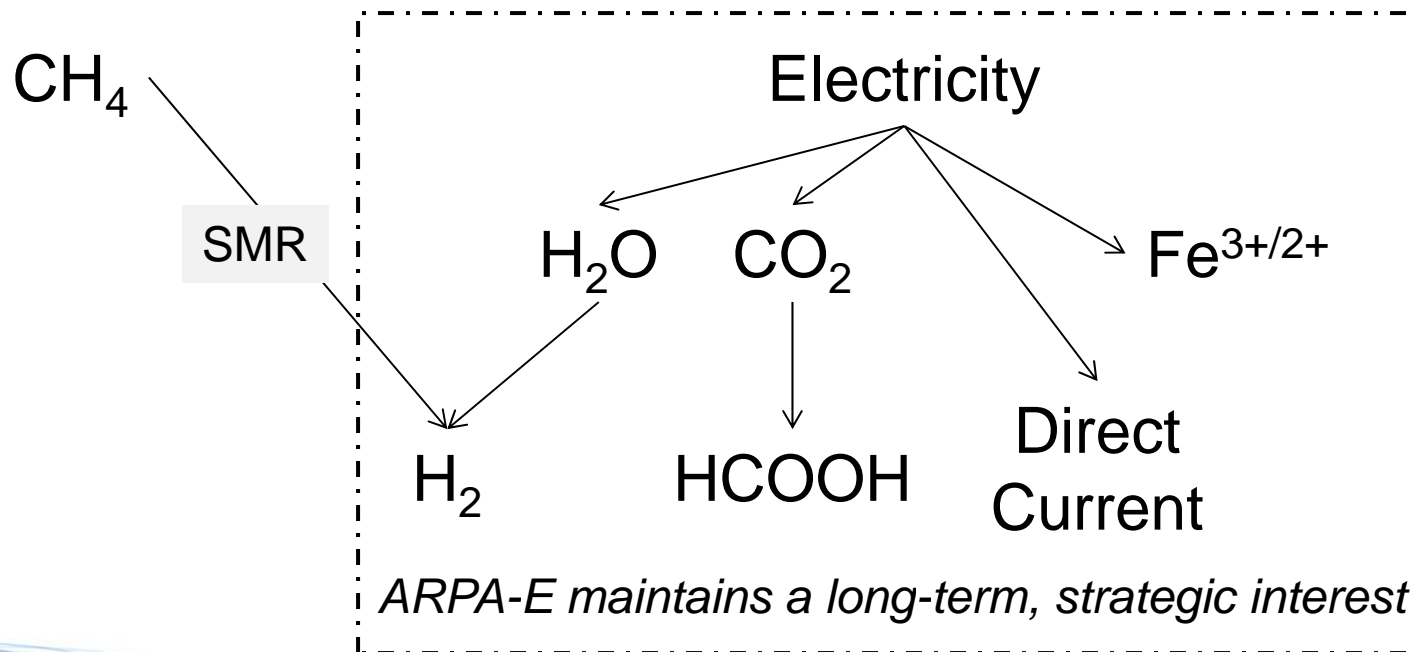
Certain feedstocks are advantaged and more near term due to particular market opportunities

## South African Company to Build U.S. Plant to Convert Gas to Liquid Fuels

By CLIFFORD KRAUSS  
Published: December 3, 2012



**sasol**  
reaching new frontiers



# ARPA-E conducted techno-economic analysis (TEA) to compare Electrofuels to other biofuel/fuel approaches

Item	Base Cost	Cost (\$/GGE)
Electricity Feedstock	\$0.04/kWh	\$2.15
Capital Cost	\$2/yearly GGE	\$0.45
CO <sub>2</sub> Feedstock	\$40/yearly CO <sub>2</sub>	\$0.37
O <sub>2</sub> Co-product	\$2	\$3
Labor and Overhead	\$0.02	\$0.06
Maintenance and Taxes	\$1	\$6
Materials and Waste	\$0	\$100
Water Feedstock	\$30	\$0
<b>Total Cost</b>	\$0.07	\$0.30
<b>Item</b>	1%	5%
Cellular Energy Efficiency	\$0.04	\$0.16
e- Consumed per Butane	\$0	\$3
Delivered Voltage	Base Cost \$3.09/GGE	100%
	25.3	\$2
	1.23	2.0



Selected representative examples where a process could be envisioned

Built general models to explore the diversity of the program

Expanded and improved the model to assess capital costs

Added precision around cost of reducing equivalents

*ARPA-E built a preliminary model to explore operating costs*

## ARPA-E and NREL specifically addressed hydrogen, formate, and direct electrosynthesis in first iteration of the models

### Hydrogen: $H_2 \rightarrow NADH, ATP + CO_2 \rightarrow$ Calvin Benson Cycle

$H_2$  can be generated from  $H_2O$  with high efficiency

High costs associated with improvements in gas mass transfer

### Formate: $CO_2 + 2H^+ + 2e^- \rightarrow HCOOH \rightarrow CO_2 + NADH + H^+ \rightarrow$ Calvin Benson

Formate is readily soluble and a source of energy and  $CO_2$

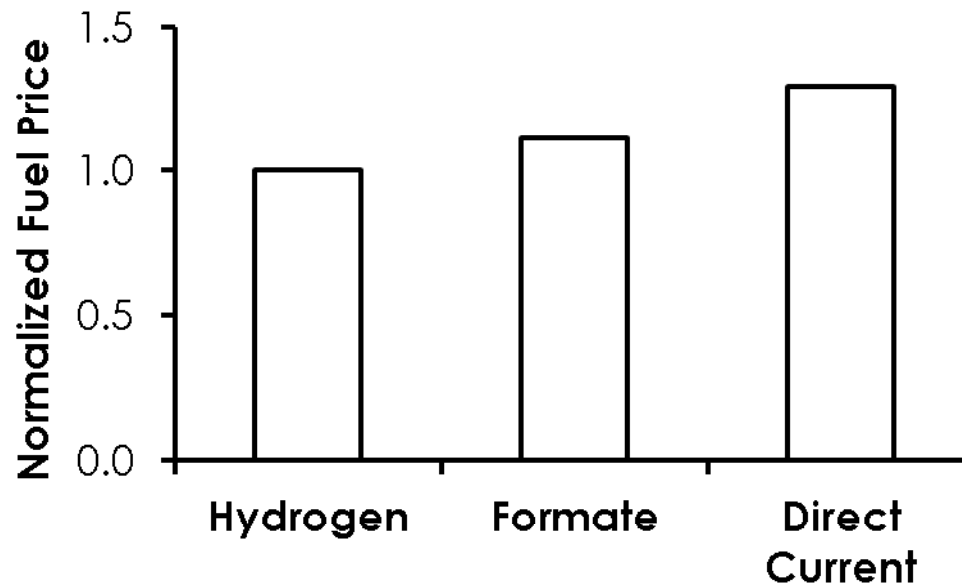
$CO_2$  reduction to formate requires large overpotential and energetic cost

### Direct Current: Direct current + $CO_2 \rightarrow$ Wood-Ljungdahl

High coulombic efficiency to acetate

Low current density and high CapEx cost

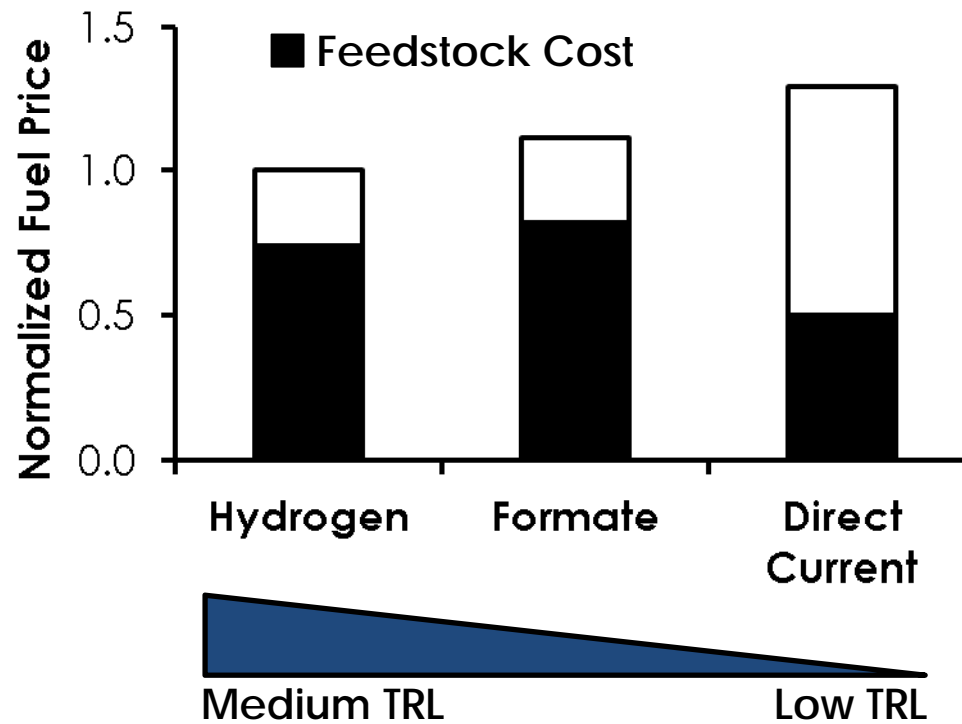
## TEA comparison of representative approaches using electricity as feedstock



- Apples-to-apples comparison using the same feedstock and producing the same final fuel molecule
- Compares the cost of assimilating electrons and fixing carbon dioxide to a final fuel



Despite TRL disparity, the target cases show similar cost of production, however feedstock dominate



Technologies are needed to reduce the cost burden of feedstocks and improve performance



# What technologies are needed to take advantage of low cost feedstock?

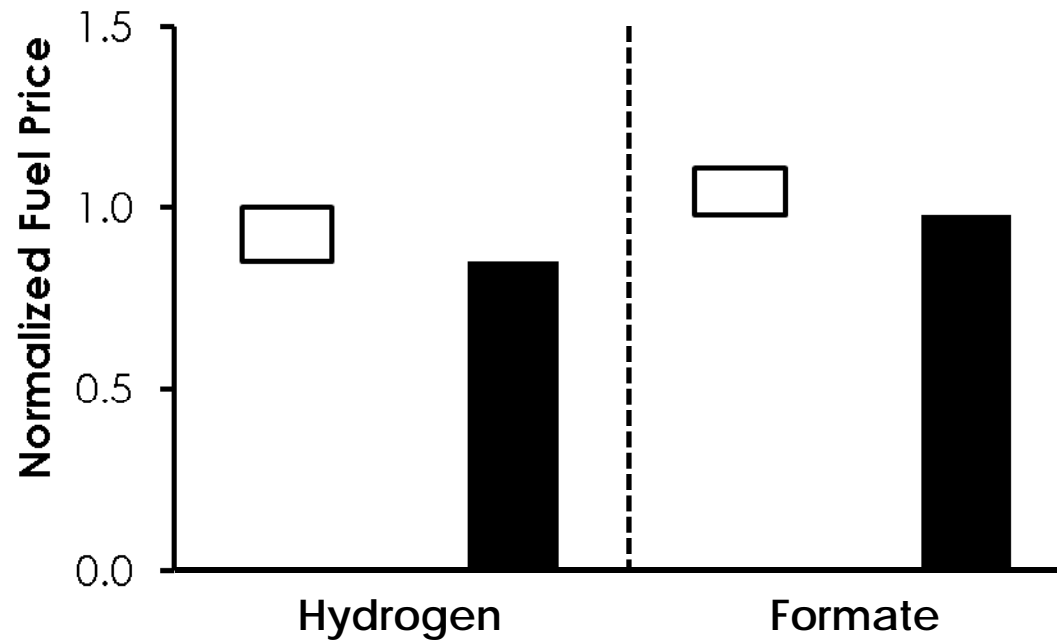
## **Efficient use of Feedstocks**

- Efficient carbon fixation pathways
- Fuel assimilation pathways with minimal ATP requirements

## **Access to Cheap Feedstocks**

- Cheap capital that can be deployed with low capacity factors
- “Energy storage” by accumulating acetate or formate with intermittent electricity supply for later conversion to fuel
- Small, modular deployment

# Relative cost savings of switching to a more efficient carbon fixation pathway



By addressing these, we can go after niche opportunities in early deployment scenarios

- **H<sub>2</sub>/CO/CO<sub>2</sub> energy source**

- Ethanol refinery bolt-on
- Geographic niches with resource availability
  - TX = cheap wind e- & EOR CO<sub>2</sub>
  - ND = natural gas processing with wind
  - Iceland & Japan = geothermal for e- and CO<sub>2</sub>

- **Electricity as energy source**

- Intermittent renewable electricity and opportunity for energy storage as formate/acetate

## Challenges and opportunities identified in the RFI

- New materials and scalable reactor technologies to improve gas to liquids mass transfer
- Development of microbial systems capable of assimilating energy from multiple sources (e.g. H<sub>2</sub>, CO, and HCOOH)
- Power/feedstock costs
- Real-time protein expression control systems
- *In situ* hydrogen generation
- Deployment opportunities targeting cheap feedstocks, resources, and permitting
- Reactor capable of operating as a dispatchable load

## Challenges to be explored in the afternoon breakout session

- **H<sub>2</sub>/CO/CO<sub>2</sub>**
  - Fuel production rates of 10 g/L/hr
  - Efficient carbon fixation pathway (e.g. not Calvin cycle)
  - High gas transfer without high pressure reactor
  - H<sub>2</sub> from CH<sub>4</sub>, biomass, e<sup>-</sup>
  - Scale to 10,000 BOE/d (150M gal/yr)

## Challenges to be explored in the afternoon breakout session

- **Formate**

- Current density of 200 mA/cm<sup>2</sup>
- Overpotential of 0.2V
- Selectivity of HCOOH::H<sub>2</sub> of 95%
- Fuel production rates of 10 g/L/hr
- Efficient carbon fixation pathway (e.g. not Calvin cycle)
- Electrochemical reactor at 1 bar
- Intermittent formate production, with continuous fuel production
- Formate accumulation of 25 g/L (production, toxicity)
- Scale to 1000 BOE/d (15M gal/yr; 70 MW)

## Challenges to be explored in the afternoon breakout session

- **Direct Current**

- Current density of 50 mA/cm<sup>2</sup>
- Overpotential of 0.2V
- Selectivity of e<sup>-</sup>::H<sub>2</sub> of 95%
- Fuel production rates of 2 g/L/hr
- Coulombic efficiency to fuel of 90%
- Intermittent electricity delivery
- Intermittent acetate production, with continuous fuel production
- Acetate accumulation of 60g/L (production, toxicity)
- Scale to 1000 BOE/d (15M gal/yr; 70 MW)